

# Adsorption Studies of Cu<sup>2+</sup> using Tea Leaves and Tea Fibre (*Camellia Sinensis*) as Adsorbents

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**Abstract:** Pollution of aquatic environments is in geometric increase and it is becoming a serious environmental problem, this pollution however includes heavy metal and they tend to threatens aquatic ecosystems, aquaculture, and directly or indirectly human health. These tend to pose danger due to their relatively high and persistent nature and accumulation and bio magnifications along the aquatic food chain. Thus this research work focuses on the removal of  $Cu^{2+}$  from aqueous solution using Tea Leaves and Tea Fibre (Camellia Sinensis) as Adsorbents. From the result of this experiment, the above named adsorbent is very efficient as it tend to 99.9% removal of the heavy metal; however it is found that the variation of pH has a negligible effect in the % removal of  $Cu^{2+}$  from aqueous solution using tea fiber and leaves, it clearly shows that tea fibre and tea leaves are good adsorbent for the removal of  $Cu^{2+}$  from aqueous solution. Therefore tea fibre and tea leaves can be employed in treatment of waste water containing  $Cu^{2+}$  for effective removal.

#### **1. INTRODUCTION**

Pollution of aquatic environments is in geometric increase and it is becoming a serious environmental problem, this pollution however includes heavy metal and they tend to threatens aquatic ecosystems, aquaculture, and directly or indirectly human health (Etim *et al.*, 2019a,b). These tend to pose danger due to their relatively high and persistent nature and accumulation and bio magnifications along the aquatic food chain (Fu *et al.*, 2014). The term "heavy metals" is often used when addressing stable and potentially toxic metals with an atomic density greater than 4g/cm<sup>3</sup> (Etim *et al.*, 2019c,d; Adelagun *et al.*, 2021; Etim et al., 2017).

Biosorption in recent times are known to be an alternative technique for the uptake of toxic metals including  $Cu^{2+}$  from wastewater (Babarinde *et al.*, 2008). However, it is a relatively new technology that has important use in the removal of low-level concentration of toxic metal (Akhtar *et al.*, 2004). Biosorption is a new technology that can be employ in the removal of metal ions from aqueous solutions, and this serve to replace the old conventional methods such as reduction or oxidation, ion exchange, filtration, electrochemical treatment, membrane technology, evaporation recovery, chemical precipitation, chemical lime coagulation and solvent extraction (Anayurt, 2009). The mechanism of the biosorption process has been explained in terms of the reaction between anionic groups present in the biomasses and the cationic metal ions (Etim *et al.*, 2019a,c).

The tea plant is the species of plant whose leaves and leaf buds are used to produce tea. It is termed as a low cost adsorbent since it requires little processing, it is abundant in nature, and a by-product from tea processing as stated by (Etim *et al.*, 2022; Bajpai *et al.*, 201; Itodo and Etim, 20150). In this research work, the tea fibre and tea leaves from tea plant are used as an absorbent.

This research work focus on the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves as an absorbent.

## 2. METHODOLOGY

#### 2.1. Sample Collection and Preparation

The tea leaves (*Camellia Sinensis*) for this research work was collected from Kakara High Land Tea, Sardauna L.G.A., Taraba State, Nigeria. They were collected into in the early hours of the day and then washed properly to remove moist and dirt, after which they were rinsed with distilled water. The sample was then properly dried at room temperature after which the sample was pulverized and sieved with 150mm micron.

### 2.2. Preparation of Stock Solution

Copper (II) oxide of 0.1M concentration was prepared and used all through the experimental work. 7.95g of copper (II) oxide powder were dissolved in 1000 mL of the stock solution.

#### 2.3. Preparation of Different Concentrations of Metal Solutions

In this research work, a total of 4 different concentrations of copper (II) oxide solutions were prepared: 20mg/l, 30mg/l, 40mg/l and 50mg/l. Subsequently, the copper solutions with different concentrations and 2g of biosorbent materials were put into an orbital shaker at different temperatures (between  $40^{\circ}c - 70^{\circ}c$ ). The rotational speed of shaker in all the experiments was kept constant at 220rpm. This experiment was performed in duplicate and the best result was used. Lastly, the solution was filtered to prepare samples for the measurements of the metal ion concentration (Etim *et al.*, 2022 and Asuquo *et al.*, 2019)

## 2.4. Effect of Initial Concentration

Metal solution of 50mL, containing different concentrations; 20mg/l, 30mg/l, 40mg/l and 50mg/l were measured into different conical flasks. 2g of the biosorbent were dispersed in each of them, the flasks were corked and the mixture agitated with the aid of a shaker for 1 hour to attain equilibrium, the slurries were then filtered using whatman filter paper and a plastic funnel, the filtrate were kept in well labeled containers and thereafter the concentrations of the resulting filtrate were determined using Atomic absorption spectrometer. (Etim *et al.*, 2022) and (Entezari, *et al.*, 2009)

#### 2.5. Effect of pH

The effects of pH on the biosorption of metal ions were carried out within the range that would not be influenced by the metal precipitated (Pavasant, *et al.*, 2006). Experiments were conducted at 30°C to study the effect of initial solution pH on the biosorption of copper (II) oxide by contacting 2g of the *camellia sinensis* with 50mL of the metal ion solution in a glass tube. The pH of each of the solutions were adjusted to the desired value with 0.1M sodium hydroxide and /or 0.1M nitric acid. The studies were conducted at pH values of 2, 3, 5 and 7. The glass tubes containing the mixture were left in a water bath for 24 h. The biomass were removed from the solution by decantation and the residual the metal concentration in the solution were analyzed

#### 2.6. Effect of Biosorbent Dosage

Biosorbent of 1g, 2g, 3g, and 4g were weighed into different conical flasks. 50ml of metal solution were measured into each of the conical flasks and labeled. The flasks were corked and the mixture agitated with the aid of a shaker for 1hour to attain equilibrium, the slurries were then filtered using Whatman filter paper and a plastic funnel, the filtrate were kept in well labeled containers and thereafter the concentrations of the resulting filtrate were determined using Atomic absorption spectrometer. (Reddad, *et al.*, 2002 and Etim, *et al.*, 2022)

#### 2.7. Isotherms Studies of Biosorption

The experimental data will be fitted using Langmuir and Freundlich (Hall et al. 1966)

#### Freundlich Isotherm

Freundlich isotherm describes an empirical relationship that exists between the adsorption of solute and the surface of the adsorbent. The empirical equation proposed by Freundlich is:

$$logq_e = logK_f + \frac{1}{n}logC$$

(2.1)

Where,

K<sub>f</sub> and n are coefficients;

qe is the weight adsorbed per unit weight of adsorbent

C is the concentration of the metal solution

taking logarithm and rearranging: logqe

$$q = K_f C^{1/n} \tag{2.2}$$

The constant  $K_f$  is an approximate indicator of adsorption capacity, while 1/n is a function of the strength of adsorption (Voudrias et al. 2002).

#### Langmuir Isotherm

The Langmuir isotherm equation is written as:

$$\frac{C_e}{q_e} = \frac{1}{q_{max}K_L} + \frac{C_e}{q_{max}}$$
(2.3)

Where,

Ce is the equilibrium concentration of adsorbate,

qe is the amount of metal adsorbed per gram of the adsorbent at equilibrium.

 $q_m$  and b are Langmuir constants related to adsorption capacity and rate of adsorption, respectively. The values of  $q_m$  and b were calculated from the slope and intercept of the Langmuir plot of C<sub>e</sub> versus C<sub>e</sub>/q<sub>e</sub> (Langmuir 1918).

#### 3. RESULTS AND DISCUSSION

# **3.1.** Effect of Initial Concentration in the Removal of Cu<sup>2+</sup> from Aqueous Solution using Tea Fibre and Tea Leaves

Table 3.1 and 3.2 shows clearly the effect of Initial concentration in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively. It was observed that as the initial concentration increases, the % removal of  $Cu^{2+}$  also increases when tea fibre and tea leaves were used as adsorbent, this shows clearly that the more the initial concentration of an aqueous solution, the more  $Cu^{2+}$  can be removed using the above named adsorbent.

In similar manner, figure 3.1 and 3.2 is a graph showing the effect of concentration in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively

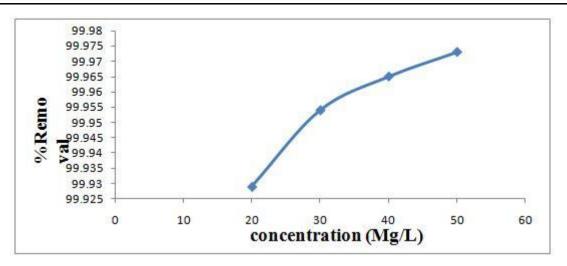
| Initial conc.             | Final conc. Mg/L          | % Removal     | Metal uptake              |  |
|---------------------------|---------------------------|---------------|---------------------------|--|
| ( <b>C</b> <sub>i</sub> ) | ( <b>C</b> <sub>f</sub> ) | (% <b>R</b> ) | ( <b>q</b> <sub>e</sub> ) |  |
| 20.00                     | 0.01418                   | 99.929        | 0.49965                   |  |
| 30.00                     | 0.01365                   | 99.954        | 0.74965                   |  |
| 40.00                     | 0.01391                   | 99.965        | 0.99965                   |  |
| 50.00                     | 0.01364                   | 99.973        | 1.24966                   |  |

**Table3.1.** Initial concentration values for the removal of  $Cu^{2+}$  from aqueous solution using tea fibre

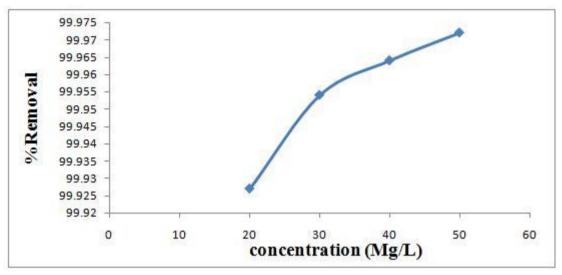
| <b>Table3.2.</b> Initial concentration values for the removal of $Cu^{2+}$ from aqueou | is solution using tea leaves |
|--|------------------------------|
|--|------------------------------|

| Initial conc. | Final conc. Mg/L | % Removal | Metal uptake  |  |
|---------------|------------------|-----------|---------------|--|
| (Ci)          | ( <b>C</b> f)    | (%R)      | ( <b>q</b> e) |  |
| 20.00         | 0.01445          | 99.927    | 0.49963       |  |
| 30.00         | 0.01364          | 99.954    | 0.74966       |  |
| 40.00         | 0.01418          | 99.964    | 0.99965       |  |
| 50.00         | 0.01377          | 99.972    | 1.24965       |  |

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**Figure3.1.** Graph of initial concentration showing the % removal of  $Cu^{2+}$  using tea fibre





3.2. Effect of pH in the Removal of Cu<sup>2+</sup> from Aqueous Solution using Tea Fibre and Tea Leaves

Table 3.3 and 3.4 shows the effect of pH in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively. It was observed that the pH of the aqueous solution have negligible effect in the % removal of  $Cu^{2+}$  when tea fibre and tea leaves were used as adsorbent, this shows clearly that the pH of an aqueous solution may not affect the % removal of  $Cu^{2+}$  using the above named adsorbent.

Similarly, figure 3.3 and 3.4 is a graph showing the effect of pH in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively

**Table3.3.** *pH* values for the removal of  $Cu^{2+}$  from aqueous solution using tea fibre

|      | 1 5                       | <i>J J</i>                | 1         | 0 5                       |  |
|------|---------------------------|---------------------------|-----------|---------------------------|--|
| pН   | Initial conc.             | Final conc. Mg/L          | % Removal | Metal uptake              |  |
|      | ( <b>C</b> <sub>i</sub> ) | ( <b>C</b> <sub>f</sub> ) | (%R)      | ( <b>q</b> <sub>e</sub> ) |  |
| 2.00 | 40.00                     | 0.01445                   | 99.964    | 0.99963                   |  |
| 3.00 | 40.00                     | 0.01377                   | 99.965    | 0.99965                   |  |
| 5.00 | 40.00                     | 0.01377                   | 99.965    | 0.99965                   |  |
| 7.00 | 40.00                     | 0.01431                   | 99.964    | 0.99964                   |  |

| <b>Table3.4.</b> p. | H values for th | e removal of Cu² | + from aqueous | solution using tea leaves |
|---------------------|-----------------|------------------|----------------|---------------------------|
|---------------------|-----------------|------------------|----------------|---------------------------|

| pН   | Initial conc. | Final conc. Mg/L | % Removal | Metal uptake              |  |
|------|---------------|------------------|-----------|---------------------------|--|
|      | ( <b>C</b> i) | ( <b>C</b> f)    | (%R)      | ( <b>q</b> <sub>e</sub> ) |  |
| 2.00 | 40.00         | 0.01404          | 99.965    | 0.99965                   |  |
| 3.00 | 40.00         | 0.01377          | 99.965    | 0.99966                   |  |
| 5.00 | 40.00         | 0.01445          | 99.964    | 0.99964                   |  |
| 7.00 | 40.00         | 0.01404          | 99.965    | 0.99965                   |  |

#### Adsorption Studies of Cu<sup>2+</sup> using Tea Leaves and Tea Fibre (Camellia Sinensis) as Adsorbents

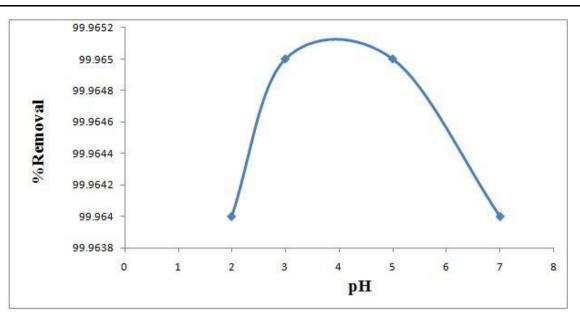
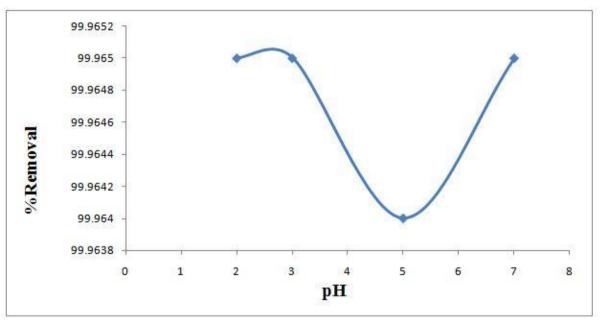


Figure 3.3. Graph of pH indicatin % removal of copper using tea fibre (Camellia Sinensis).



**Figure3.4.** *Graph of pH indicating % removal of copper using tea leaves* 

# **3.3.** Effect of Adsorbent Dosage in the Removal of Cu<sup>2+</sup> from Aqueous Solution using Tea Fibre Tea Leaves

Table 3.5 and 3.6 shows the effect of adsorbent dosage in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively. A decrease of % removal was obseved at a high adsorbent dosage when tea fibre and tea leaves were used as adsorbent, this shows clearly that at high adsorbent dosage, the % removal of  $Cu^{2+}$  will be reduced using the above named adsorbent.

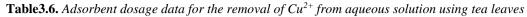
Similarly, figure 3.5 and 3.6 is a graph showing the effect of adsorbent dosage in the removal of  $Cu^{2+}$  from aqueous solution using tea fibre and tea leaves respectively

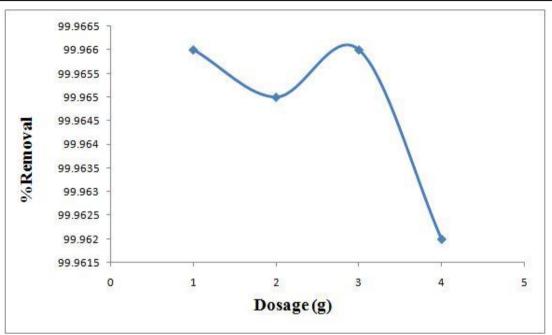
**Table3.5.** Adsorbent dosage data for the removal of  $Cu^{2+}$  from aqueous solution using tea fibre

| Adsorbent<br>dosage(g) | Initial conc.<br>(C <sub>i</sub> ) | Final conc. Mg/L<br>(C <sub>f</sub> ) | % Removal<br>(%R) | Metal uptake<br>(qe) |  |
|------------------------|------------------------------------|---------------------------------------|-------------------|----------------------|--|
| 1.00                   | 40.00                              | 0.01377                               | 99.966            | 1.99931              |  |
| 2.00                   | 40.00                              | 0.01404                               | 99.965            | 0.99965              |  |
| 3.00                   | 40.00                              | 0.01377                               | 99.966            | 0.66644              |  |
| 4.00                   | 40.00                              | 0.01526                               | 99.962            | 0.49981              |  |

#### Adsorption Studies of Cu<sup>2+</sup> using Tea Leaves and Tea Fibre (Camellia Sinensis) as Adsorbents

| Adsorbent<br>dosage(g) | Initial conc.<br>(C <sub>i</sub> ) | Final conc. Mg/L<br>(C <sub>f</sub> ) | % Removal<br>(%R) | Metal uptake<br>(q <sub>e</sub> ) |  |
|------------------------|------------------------------------|---------------------------------------|-------------------|-----------------------------------|--|
| 1.00                   | 40.00                              | 0.01364                               | 99.966            | 1.99932                           |  |
| 2.00                   | 40.00                              | 0.01364                               | 99.966            | 0.99966                           |  |
| 3.00                   | 40.00                              | 0.01431                               | 99.964            | 0.66643                           |  |
| 4.00                   | 40.00                              | 0.01364                               | 99.966            | 0.49983                           |  |





**Figure3.5.** Graph showing adsorbent dosage for % removal of  $Cu^{2+}$  using tea fibre

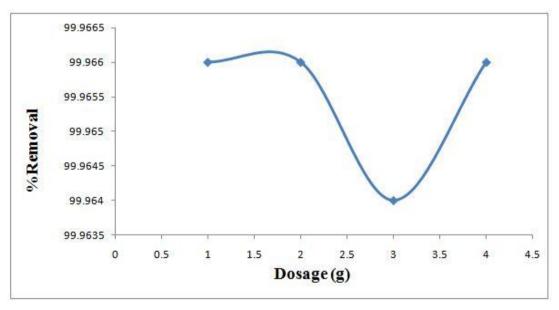


Figure3.6. Graph showing adsorbent dosag for % removal of copper using tea leaves

#### **3.4. Freundlich Isotherm and Langmuir Isotherm**

The adsorption constants and the correlation coefficients for the two isotherm models are presented in table 3.7 and 3.8 where  $K_L$  and  $K_f$  is the adsorption capacity and  $q_{max}$  and 1/n the adsorption intensity. This indicate the relative distribution of energy and heterogeneity of adsorbate sites for Langmuir and Freundlich model and considering the distribution, the Langmuir model described the adsorption process better than Freundlich model. The R<sup>2</sup> values for the two models also indicate Langmuir to be better. The R<sub>L</sub> values which are called the separation factor explain the adsorption to be irreversible.

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| Conc. (Mg/L) | logCe<br>(leaves) | logq <sub>e</sub><br>(leaves) | logCe<br>(fibre) | logqe<br>(fibre) |  |
|--------------|-------------------|-------------------------------|------------------|------------------|--|
| 20           | -1.8401           | -0.3013                       | -1.8483          | -0.3013          |  |
| 30           | -1.8652           | -0.1251                       | -1.8652          | -0.1251          |  |
| 40           | -1.8483           | -0.0002                       | -1.8567          | -0.0002          |  |
| 50           | -1.8611           | 0.0968                        | -1.8652          | 0.0968           |  |

 Table3.7. Freundlich isotherm data for tea leaves and fibre

**Table3.8.** Langmuir isotherm data for tea leaves and fibre

| Conc. (Mg/L) | Ce/ qe   | Ce       | Ce/ qe  | Ce      |  |
|--------------|----------|----------|---------|---------|--|
|              | (leaves) | (leaves) | (fibre) | (fibre) |  |
| 20           | 0.029    | 0.01445  | 0.028   | 0.01418 |  |
| 30           | 0.018    | 0.01364  | 0.018   | 0.01364 |  |
| 40           | 0.014    | 0.01418  | 0.014   | 0.01391 |  |
| 50           | 0.011    | 0.01377  | 0.012   | 0.01364 |  |

**Table3.9.** Isotherm parameters for the adsorption of  $Cu^{2+}$  using tea fibre and leave at different concentrations

| Isotherm   | Parameters              | Biosorbent |
|------------|-------------------------|------------|
| Langmuir   | q <sub>max</sub> 21.549 | Fibre      |
|            | K <sub>L</sub> -0.2803  |            |
|            | $R^2$ 0.6124            |            |
|            | R <sub>L</sub> 0.9962   |            |
| Freundlich | 1/n -15.259             |            |
|            | K <sub>f</sub> -28.446  |            |
|            | $R^2$ 0.5165            |            |
| Langmuir   | q <sub>max</sub> 14.005 | Leave      |
|            | K <sub>L</sub> 0.1782   |            |
|            | $R^2$ 0.4397            |            |
|            | R <sub>L</sub> 0.9961   |            |
| Freundlich | 1/n -8.3968             |            |
|            | K <sub>f</sub> -15.647  |            |
|            | $R^2$ 0.3192            |            |

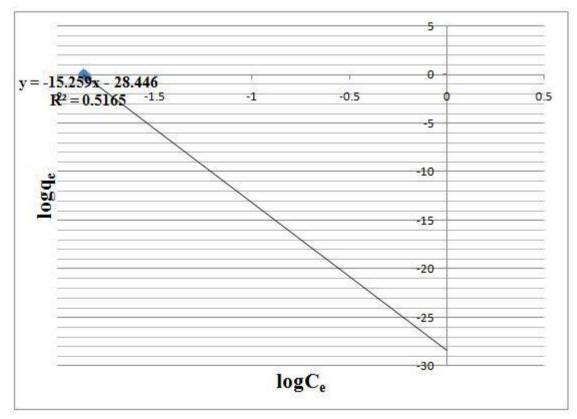


Figure 3.7. Freundlich isotherm graph for tea fibre

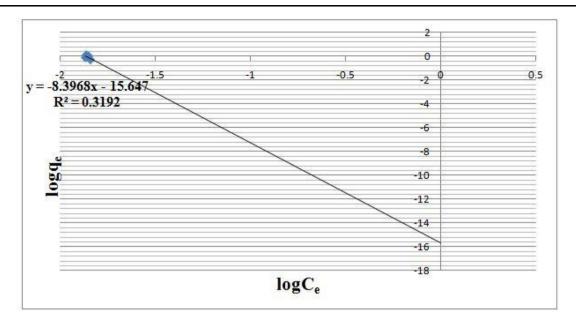


Figure 3.8. Freundlich isotherm graph for tea leave

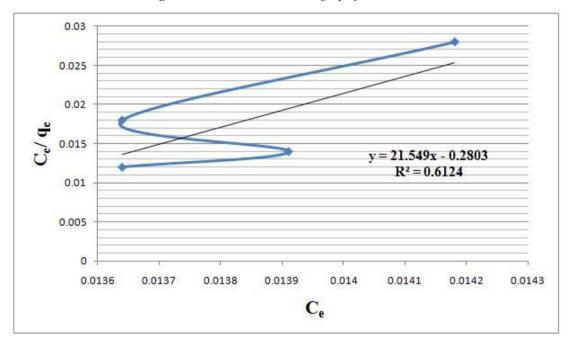


Figure 3.9. Langmuir isotherm graph for tea fibre

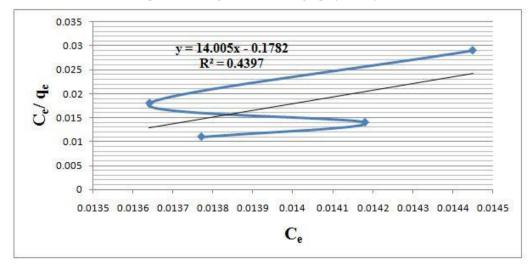


Figure 3.10. Langmuir isotherm graph for tea leave

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#### 4. CONCLUSION

From the results obtained in this show that tea fibre and tea leaves can be used can good adsorbents for the removal of  $Cu^{2+}$  in the treatment of domestic wastewaters and industrial effluents.

The maximum percentage removal of  $Cu^{2+}$  was found to 99.97% in both adsorbents. This further attests to the high the high accuracy and efficiency of the adsorbent used. In conclusion, since both the tea fibre and tea leaves are found to be good biosorbents which are occur naturally and are environmentally friendly, these adsorbents should be adopted in the treatment of wastewaters and industrial effluents.

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